

Malonate Complexes at γ -Alumina Surface Determined by a Multitechnique Characterization Approach and a Surface Complex Model

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2 technique characterization approach and a surface complex model

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11 Abstract

12 y-Al₂O₃ is a transition alumina oxide used in many different applications. Its surface chemistry 13 seems to be a key factor in the preparation of heterogeneous catalyst where γ -Al₂O₃ is used as a support. The modification and description of its surface are necessary to understand the role of the 14 15 support on the catalyst preparation and on its performance. In this work, the modification of the 16 surface is performed with a carboxylic diacid, malonic acid, which specifically adsorbs at the y-Al₂O₃ 17 surface and modifies the surface chemistry (surface sites density and global surface charge). The impact 18 of the impregnation pH, malonic acid content, and drying are studied. By using a multi-technique 19 approach, both the solid/liquid interface and the dried surface were characterized. The infrared 20 spectroscopic information coupled with zetametry measurements indicate the formation of an inner 21 sphere complex adsorbed via both side-on ester linkage and bridging bidentate mode involving the two 22 carboxylic groups. A surface complexation model was built to support the experimental results and 23 obtain complementary information. It underlines the different reactivity of the y-Al₂O₃ facets and of the 24 surface sites responsible for the adsorption. The whole (100) facet is involved in the adsorption while 25 only the μ_1 -Al_V-OH and μ_1 -Al_V-OH sites of the (110) facet participate in the malonic acid adsorption. The 26 model also confirms the consumption of 3 to 4 surface hydroxyls per adsorbed molecule, in accordance 27 with ester linkage and bridging bidentate structure. This molecular level description of the surface 28 chemistry is of interest in different environmental fields such as wastewater treatment and pollutant 29 removal. In the catalysis field, the detailed surface chemistry will be very useful to understand the 30 impact of this modified support on the catalytic performance.

31 <u>Keywords</u>

32 Malonic acid, gamma-alumina, surface complexation models, solid/solution interface, PhreeqC

33 Introduction

34 The interaction between organics and metal (hydr)oxides surface is of interest in many application fields 35 such as environmental chemistry (pollutants removal through adsorption¹), chemical waste treatments², and catalysis (e.g. hydrotreating catalyst^{3,4}). For this latter application, the strong 36 37 interaction between the active phase of the catalyst and the support is often mentioned to play a key role on the final catalytic activity^{5–8}. By adding an organic additive during the catalyst preparation, this 38 39 active phase-support interaction can be tuned, with a strong impact on the performance. Thus, the 40 identification of complexes adsorption on metal (hydr)oxides surface at the solid/liquid interface at a 41 molecular level is a real challenge both from a fundamental and from an industrial point of view.

42 The interaction of organic acids with γ -Al₂O₃ is of particular interest for catalyst preparation since this support is widely used in heterogeneous catalysis, for example in case of hydrotreating and Fischer-43 Tropsch catalysts^{9,10}. Indeed, carboxylic acids used as an additive during the catalyst preparation can 44 45 positively impact the catalytic performance¹¹. This increased activity could be explained by a delayed sulphidation³ (activation stage of the catalyst), a better dispersion or a weakened interaction with the 46 support due to metal precursors' complexation¹² by the additive. Another role the additive could play, is 47 48 the modification of the surface chemistry of the support which will in turn impact the active phase support interaction. The ability of carboxylic acid to strongly modify the alumina surface by specific 49 bonding¹³⁻¹⁵ could be a useful property in order to understand the role of the support during catalyst 50 preparation. As an example, one of the most studied carboxylic acid additive, citric acid^{16–18}, has proved 51 to increase the catalytic activity when pre-impregnated onto the support¹⁹. However, intrinsic 52 53 properties of citric acid such as its tendency to favour metals reduction^{20,21} or complexing properties 54 with both, the promoter and active phase precursor depending on the solution pH⁴ added to its possible degradation²² make it difficult to rationalize the role of the support. In that sense, malonic acid, rarely 55 studied in the hydrotreatment field (sometimes evocated as an additive²³ or rejuvenation agent for 56 spent catalyst^{24–26}), is a valuable candidate as it adsorbs specifically at the y-Al₂O₃ surface^{2,13,27} and does 57 58 not interact with metallic precursors or degrade at the surface. In this work, malonic acid has been 59 chosen to tune the surface chemistry of catalyst support.

60 Consequently, the description at a molecular level of the y-Al₂O₃ surface modified by malonic acid represents a first important step in the characterization of the role of the support for further 61 62 heterogeneous catalysts preparation and performance studies. This system has already been studied 63 using in situ attenuated total reflection-infrared spectroscopy, ATR-FT-IR. Using the latter technique, 64 Dobson et al.¹³ have proposed that adsorption takes place through ester linkage via the two carboxylic 65 groups. However, in a recent study on the interaction of europium (III) with γ -Al₂O₃ in the presence of malonic acid, Patel et al.², based on ATR-FT-IR and Time Resolved Fluorescence spectroscopic data, 66 67 proposed the formation of a bidentate mononuclear complex as well as a protonated bidentate species, 68 involving two and one carboxylic groups, respectively. This shows that the geometry of the complex is 69 still not clearly defined. Moreover, these research works focus on the solid/liquid interface while a 70 further drying stage is applied during the catalyst preparation and might impact the geometry of the 71 complex. Finally, these previous studies are focused on the geometry of the adsorbate, but the 72 adsorption sites involved in the malonic complex formation at the y-Al₂O₃ surface were not investigated. These two features (evolution during drying and reactive sites) are essential in theunderstanding of the role of the support in catalysis and are addressed in this study.

75 In the present work, the modification of the γ -Al₂O₃ surface chemistry induced by the impregnation of 76 malonic acid at different contents (from 0.2 to 0.9 malonic acid/nm²) is described. The adsorption at the 77 solid/liquid interface was quantified by adsorption isotherms and was probed by in situ ATR-FT-IR and 78 zetametry techniques. The impact of a drying stage on the geometry of the surface complexes is also 79 discussed based on infrared spectroscopy characterizations. Finally, by using the information derived 80 from the characterizations, a surface complexation model has been built based on a DFT description of the hydrated alumina surface²⁸⁻³¹ and the MUSIC model³². This simulation is an approach we have 81 82 developed to support the experimental data and obtain complementary information on the complex 83 geometry, the reactivity of γ -Al₂O₃ faces and of the surface sites involved in the adsorption process.

84 Experimental/method Section

85 Adsorption isotherm/ ionic chromatography

The support was prepared by peptization of AlOOH boehmite Pural SB3 (purchased from Sasol) with concentrated nitric acid, molding by extrusion and calcination in air at 540°C for 4 hours. These γ -Al₂O₃ extrudates were crushed to obtain particles between 400 and 800 µm in order to avoid diffusion limitations. The support had a surface area of 209 m² g⁻¹ determined by nitrogen physisorption and a pore volume of 0.88 cm³ g⁻¹.

91 The adsorption isotherm of malonic acid was measured under atmospheric conditions by contacting y-92 Al_2O_3 with solutions of different initial concentrations at constant temperature, 25°C and at pH 4.2 grams of solid were introduced in a batch reactor containing a volume of solution equal to ten times the 93 94 pore volume, i.e. 17.6 mL, at a specific concentration of malonic acid and pH. Then, it was stirred for 3 95 hours to assure the equilibrium as it is usually reached in less than an hour for the system carboxylic acid/alumina^{2,33}. During the experiment, the pH was checked every 30 minutes and maintain at 4 by the 96 97 addition of a small volume of HNO₃ (10⁻¹ mol L⁻¹, Fischer Scientific). The initial solution concentration of malonic acid (99%, VWR reagents) ranged from 5.10^{-3} to $2.5.10^{-1}$ mol L⁻¹ and its pH was adjusted by a 98 99 solution of NaOH (0.1 mol L⁻¹, VWR reagents). It is worth noted that the ionic strength was not control 100 by the addition of an electrolyte for all solid/solution experiments. Indeed, the main purpose of the y-101 Al₂O₃ surface modification is to prepare catalyst's support. However, addition of foreign ions, such as 102 Na⁺, represents a poison for the catalyst and thus their addition has been excluded.

Both initial and final concentration of malonic acid were measured by ionic chromatography. This quantification was performed on an ECO IC (Metrohm) using a Shodex IC-SI-354D analytical column (150 mm length x 4 mm I.D.) at 45°C with isocratic 3.6 mM Na₂CO₃ eluent at a flow rate of 1.2 mL min⁻¹. The differences between the initial and the final concentration gives access to the malonic acid content at the surface. After the adsorption isotherm and a filtration step, a drying of the solids (120°C, 6h) is applied. Then, each solid is divided into two parts. The first part of the solid was used to perform the zetametry measurements. For the second part, a washing step was performed with distilled water
 (2x10mL) to measure the quantity of released malonic acid in solution by rinsing. The same
 quantification procedure with ionic chromatography was used to determine the surface coverage.

112 Sample preparation by incipient wetness impregnation (IWI)

113 Several solids were prepared by incipient wetness impregnation³⁴ (IWI) in order to control the surface 114 coverage of malonic acid (0.2, 0.6 and 0.9 molecule/nm²) and further FT-IR characterizations. The 115 crushed extrudates used as supports are the same as those used for the adsorption isotherm. As a 116 starting reagent malonic acid was dissolved in water and the pH adjusted at 4 by NaOH (0.1 mol L⁻¹). The 117 impregnation solution concentration ranged from 7.5.10⁻² to 2.9.10⁻¹ mol L⁻¹ to reach the targeted 118 coverage. Another solid was impregnated to reach the value of the experimental monolayer (0.9 119 molecule/nm²) with a solution adjusted at pH 6.8 with NaOH. For each coverage, 5 grams of γ -Al₂O₃ 120 were impregnated by 4.4 mL of the impregnation solution. The solid was placed under a saturated 121 water vapour atmosphere for 16 hours for an aging stage and then dried at 120°C for 6 hours.

122 ATR-FT-IR in/ex situ

The ATR-FT-IR spectra were collected in the range 4000-650 cm⁻¹ with a dry-air-purged Thermo 123 124 Scientific Nicolet IS50 FT-IR equipped with a MCT-B detector. Spectral resolution was 4 cm⁻¹ and spectra 125 were averaged from 256 scans. The crystal used was a single reflection diamond/ZnSe crystal with an 126 incidence angle of 45°C (Smart PIKE). In order to maximize the contact between the sample and the 127 crystal, the sample was crushed to powder before deposition on the crystal and then pressed onto the 128 crystal during the analysis. Data processing was carried out using OMNIC software. All spectra were 129 treated using the same procedure: atmospheric correction, advanced ATR correction and automatic 130 baseline correction between 900 and 18500 cm⁻¹.

131 The *in situ* ATR-FT-IR spectra were collected with the same spectrometer and recording parameters. First, the horizontal diamond/ZnSe crystal was coated with 1 μ L of a γ -Al₂O₃ suspension (1 g L⁻¹) which 132 133 was dried under a flow of N₂. This procedure was repeated twice. A flow cell was clamped on the ATR 134 accessory. In order to stabilize the coating, distilled water adjusted at pH 4 with HNO_3 (1 M) was flushed 135 on the oxide film with a constant flow rate of 1 mL min⁻¹ using a peristaltic pump (Ismatec S.A.) at room 136 temperature. After 30 minutes, the stabilization of the coating was checked by the absence of 137 difference between two consecutive spectra, the background spectrum was then recorded and a 138 malonic solution (10^{-3} mol.L⁻¹) adjusted at pH between 9 and 4 by NaOH or HNO₃ (0.1 mol L⁻¹) was used 139 as the circulating solution.

140 Transmission FT-IR Spectroscopy

141 The FT-IR spectra were collected using a Vertex 70 spectrometer in the 4000-400 cm⁻¹ range. Spectral 142 resolution was 4 cm⁻¹ and spectra were averaged with 32 scans. The powdered samples of 143 approximately 20 mg were pressed into self-supporting pellets of 16 mm in diameter. The samples were 144 activated at 120°C under high vacuum (< 10^{-5} mbar). This condition allowed to prevent the degradation of organic molecules but did not remove all the physisorbed water from the alumina surface. Dataprocessing was carried out using OMNIC and Origin software.

147 Zetametry measurements

148 The zeta potential measurements were performed using a Malvern Nano ZS Zetasizer. Zeta potentials 149 were calculated from measured electrophoretic velocity rates using the Smoluchowski equation. Before the measurement, the dried solid was grounded in order to obtain powder and avoid the settling 150 151 problem. Thus, measurements were carried out using 100 mg of powdered samples suspended in 100 152 mL of aqueous solutions under stirring. The pH of the suspension was adjusted with 0.1 M HNO₃ and 0.1 153 M (or 0.01 M) NaOH solutions (prepared from VWR commercial solutions). The starting pH was adjusted 154 around 3. After a few minutes of equilibration, an aliquot was withdrawn and analyzed using the Zetasizer. It was then poured back in the reactor. After adjusting the pH with NaOH, a new aliquot was 155 156 withdrawn when the pH value was stable. The protocol was repeated until pH reached a value of 157 approximately 10.

158 PHREEQC Modelling

PHREEQC2 speciation software was used to model the zetametry curve progression with increasing malonic acid coverage. As in a previous study³⁵, the acido-basic equilibria at the alumina surface determined by Corral Valero *et al.*³² have been used with basic Stern model as an electrostatic model with a capacitance of 1.39 F/m² and ion pair formation constant (log K) of 0.096 for Na⁺ and 0.176 for Cl⁻ based on the parameters used by Mayordormo *et al.*³⁶

164 The zeta potential values cannot be calculated with accuracy due to the difficulty to locate the shear 165 plane, so its experimental value was compared to the value of the potential at the Stern plane (ψ_1), near 166 to the shear plane but located slightly closer in the diffuse layer³⁷. Nevertheless, Stern and shear plane 167 potentials coincide when their value is close to zero.

Since the adsorption of malonic acid was shown to be irreversible (after drying), the sorption equilibrium was not implemented in the PHREEQC code. The protocol which was followed was to replace a given fraction of hydroxyl sites by a surface adsorption complex, according to the stoichiometry of the assumed adsorption reaction and the surface density of adsorbed malonate. For the solution equilibria, the database Thermoddem v1.10 has been used, completed by the deprotonation equilibria with malonic acid³⁸. An example of the PHREEQC code used for a malonic content of 0.9 molecule/nm² is given in the supporting information (PHREEQC Script).

175

176

178 **Results/discussion**

179

180 Solution speciation

181 Malonic acid is a dicarboxylic acid with two protonation constants, leading to three possible species as a 182 function of the pH. The pH chosen to perform the impregnation is thus of high importance. As shown in 183 Figure 1.A, the diprotonated species (AH₂) dominates for the most acid solutions (pH<2.8), the 184 monoprotonated species (AH⁻) for intermediary pH, between the two pKas (2.8<pH<5.3) and the

185 dicarboxylate (A^{2-}) for the most basic solutions (pH>5.3).



186

187Figure 1 : (A) Speciation diagram of malonic acid forms in solution calculated with PHREEQC (B) ATR-FT-IR spectra of malonic188acid solution at C= 10⁻¹ mol L⁻¹ at pH 1.4, 4.0 and 7.3 in the 1800-1100 cm⁻¹ area

189 The infrared signature of the three species differs mainly because of their protonation degree (Figure 190 1.B). The di- and monoprotonated acids have a HO-C=O group in common giving rise to an intense band around 1720 cm⁻¹ ($v_{C=0}$). Other strong infrared bands can be found in the 1590-1560 cm⁻¹ range and 191 192 around 1375-1350 cm⁻¹, which corresponds respectively to the asymmetric and symmetric stretchings 193 of carboxylate COO⁻ group present in both the deprotonated and partially deprotonated malonic acid. 194 Between the spectra of the solution at pH 4 and the one at pH 7.3, a red shift is observed for both asymmetric and symmetric stretchings (1585 to 1565 cm⁻¹ and 1375 to 1358 cm⁻¹, respectively). This is 195 due to the complete deprotonation of the diacid. The last band of interest in this region is the one at 196 197 1430 cm⁻¹ assigned to the CH₂ bending mode. The spectrum recorded at pH 4 possesses characteristic 198 band for both carboxylic and carboxylate groups. Less intense bands are observed at 1258 cm⁻¹, attributed to a CH₂ bending mode, one at 1218 cm⁻¹, attributed to C-OH stretching and finally one at 199 200 1170 cm⁻¹, which is attributed to CCH bending^{13,39}

The different spectral signatures observed in solution give a first indication on the way to differentiate the protonated and deprotonated forms of malonic acid before interacting with the γ -Al₂O₃ surface. Nevertheless the geometry of the molecule can drastically change once adsorbed at the surface⁴⁰, and the spectra of the adsorbates can be very different from any dissolved species.

In this article, the term "malonic acid" encompasses the three protonation states (diacid, anionic monoacid and dianion whose distribution is plotted in Figure 1) to simplify the writing. When it refers to the diacid molecule, it is specified in the text.

208 Solid/liquid interface characterization

The adsorption process of malonic acid has been followed by an *in situ* ATR-FT-IR experiment as a function of pH. The *in situ* experiment can track any change in the complex adsorption mode or geometry induced by a modification of the solution pH and can thus help to determine the adsorption mode of the complex formed at the alumina surface and the potential influence of the pH. The figure 2 presents the evolution of the infrared signal when the pH is changed from 9 to 4 (Figure 2.A) and back from 5 to 9 (Figure 2.B).



Figure 2 : *in situ* ATR-FT-IR spectra of the sorption of malonic acid from a solution at C = 10⁻³ mol L⁻¹ as a function of pH. (A)
 from pH 9 to 4 and (B) from pH 4 to 9.6.

218 The intensity of the signal evolves but the spectral signature remains unchanged on the whole pH range 219 except for the return to pH 9 where the signal shape changes. This observation suggests the presence of 220 a unique adsorption mode irrespective of the solution pH (at least in the range of pH = 4 to 7). 221 Moreover, the spectra have the same spectral signature as the one recorded at even lower pH value 222 (pH=2) found in the literature². This information confirms that the surface complex is insensitive to 223 values lower than the first protonation constant (pka1=2.8). The evolution of the signal indicates a 224 favoured adsorption of malonic acid at acidic pH since the intensity increases when the pH decreases 225 (Figure 2.A). On the opposite, the signal decreases when the pH is increased (Figure 2.B), indicating a 226 desorption process due to pH change when no drying stage is applied. The lowest pH value was limited 227 to 4 in order to avoid the support's dissolution. However, a decreasing intensity would be expected at 228 lower pH, as it is observed for malonic acid adsorption on anatase or lepidocrocite⁴¹.

In any case, *in situ* ATR-FT-IR, as expected⁴¹, proved that malonic acid adsorbs specifically on alumina.
 The geometry of the adsorbed complex at the solid/liquid interface (further discussed) does not depend

on the starting solution pH but the amount of adsorbate does, with an optimum pH in our study range
 around 4. Consequently, this pH value has been used to measure an adsorption isotherm. The Figure 3
 presents the adsorption isotherms before and after a washing stage determined by ionic
 chromatography.



235

Figure 3 : Adsorption isotherms of malonic acid at the alumina surface performed at pH=4 and room temperature, 3h
 equilibrium impregnation. Estimated error : ± 5%

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The isotherm exhibits a plateau around 0.9 molecule/nm² after the washing stage which indicates the quantity required to form a malonic acid monolayer at the alumina surface. These isotherms also confirm a strong interaction of the malonic acid with the surface since it starts to adsorb at low concentration. The weak impact of the washing stage indicates that most of the malonic acid molecule is adsorbed specifically by forming an inner sphere complex and only a small amount would form an outer-sphere complex or be adsorbed electrostatically onto the surface.

245

$$Q = \frac{Q_{max}K_LC_{eq}}{1+K_LC_{eq}}$$
 (eq.1)

247

The Langmuir model has been used in order to fit the experimental data. It is represented by equation 1 where Q is the equilibrium amount of adsorbed malonic (mol g^{-1}), C_{eq} is equilibrium concentration of malonic acid in solution (mol L^{-1}), Q_{max} (mol g^{-1}) is the maximum adsorption capacity and K_L the Langmuir constant. The fit was realized following a least squares procedure. Q_{max} was converted to N_{max} in molecule/nm² using the specific surface of the support (209 m² g⁻¹). The Langmuir constant gives an indication on the adsorption strength. The Langmuir isotherm parameters presented Table 1 are in the

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same order of magnitude than other acids, such as acetic and propionic acid, adsorbed on α -alumina³³ but the Q_{max} for these monoacids (Table 1) is around 50% higher, probably due to the size of the molecule and steric hindrance. A stronger affinity, higher K_L (Table 1), could be explained by a chelation effect, since malonic acid has two carboxylic groups.

258

259Table 1 : Langmuir fitting parameters for the isotherms before and after washing stage compared to Langmuir parameters of
acetic and propionic acid adsorption on α-Al₂O₃ from literature³³

Isotherm	Q _{max} (mol g⁻¹)	K∟ (L mol⁻¹)	R²	N _{max} (molecule/nm²)
Before washing	3.89x10 ⁻⁴	114	0.956	1.08
After washing	3.33x10 ⁻⁴	193	0.908	0.94
Acetic acid on α -Al ₂ O ₃	6.1x10-4	45	0.966	/
Propionic acid on α-Al ₂ O ₃	6.4x10-4	61.6	0.990	/

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The *in situ* ATR-FT-IR characterization and adsorption isotherm give a first insight into the adsorption process of malonic acid at the solid/liquid interface. However, during a catalyst preparation using a preimpregnation step a drying stage is often applied before the impregnation of active phase precursors. The adsorption mode of malonic acid could be impacted and needs to be determined after a drying

200 The adsorption mode of majoric acid codid be impacted and needs to be determined a

stage and a subsequent creation of a solid/liquid interface during the impregnation.

268 Adsorption mode of malonic acid

Several adsorption modes of the protonated and deprotonated forms of malonic acid on mineral oxides surface are given in the literature⁴¹ (Figure 4). These modes differ by the number of carboxylate groups adsorbed at the metal oxide surface (one or two), the number of aluminum surface site involved, and

the number of oxygen atoms per aluminum atom involved.



Figure 4 : Potential adsorption modes for malonic acid adsorbed on alumina surface (modified scheme from Hug et al.⁴¹)

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Structures (1), (2) and (3) involve one carboxylate group, all the others involve two carboxylate groups (except for the outer-sphere hydrogen bonded complex (6)). Each carboxylate group can create one bond with one aluminum atom (monodentate), two bonds with the same aluminum atom (bidentate chelating) or each oxygen of the carboxylate group can create a bond with a different aluminum site (bidentate bridging).

As the impregnation isotherm indicates a specific adsorption, the surface sites density and charge should be impacted, and this modification can thus be monitored by zetametry. The Figure 5 presents the evolution of the zeta potential as a function of the pH and the malonic acid content.



Figure 5 : Zeta potential as a function of pH for different surface coverages of malonic acid from 0 to 0.9 molecule/nm² (lines are used as guidance for the reader)

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288 The isoelectric point (IEP) of a solid (pH at $\zeta=0$ mV) is the result of the surface charge developed by the 289 surface sites and is characteristic of the oxide composition and structure. The change in the density of 290 surface hydroxyls by the specific adsorption of anionic species leads to a shift of the IEP towards lower 291 values^{42,43}. However, malonic acid has a peculiar impact on the zeta potential. Above 0.8 292 molecules/nm², a plateau in the zetametry curves starts to appear. At monolayer coverage, the plateau 293 has a zeta potential of zero and extends from pH 5.5 to 8. This observation indicates the presence of a neutral surface complex with both carboxylate moieties bounded to the surface⁴⁴. Indeed, an ionisable 294 295 moiety would have led to the formation of a negative surface charge by deprotonation reaction (pKa₂ is 296 equal to 5.3, see Figure 1) which is not compatible with a neutral zeta potential for a wide range of pH 297 values. Thus, the adsorption modes (1), (2) and (3) can be discarded among the different mechanisms 298 proposed in the literature (Figure 4). It should be noted that complete neutralization is only reached at 299 full monolayer coverage.

In an attempt to better understand the mechanisms, ATR-FT-IR spectra of the solution of malonic acid at pH 4 (impregnation pH) have been compared to an *in situ* spectrum recorded at pH=4 (from Figure 2) and to the one of the solid prepared by IWI and dried at 120°C (Figure 6). It should be noted that the dried and *in situ* spectra correspond to different surface coverage, 0.9 and 0.2 malonic acid/nm², respectively. However, they could be compared as it could be considered that the surface speciation does not evolve with the surface charge.



Figure 6 : ATR-FT-IR spectra of (a) malonic acid solution C=0.1 mol L⁻¹ at pH =4 (b) malonic adsorbed on the alumina deposit
 (in situ experiment at pH 4) and (c) malonic acid adsorbed on γ-Al₂O₃ by IWI (pH 4, 0.9 molecule/nm² and dried at 120°C for
 6 hours). All spectra are normalised to highest data point of each spectrum.

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311 As already observed in the Figure 2, the malonic acid adsorption induces some spectral changes and the 312 clear difference between the spectra of the solution and the complexes adsorbed on alumina (in situ or 313 dried) supports a specific adsorption. First of all, the stretching mode of the HO-C=O (1720 cm⁻¹) is not 314 present after adsorption indicating its participation to the adsorption process and thus its absence in the complex formed at the surface⁴¹. Then, adsorption modes schematized by structure (4), (5) and (9) 315 in Figure 4 can be discarded. Secondly, the symmetric stretching mode of the COO group is shifted to 316 lower value, from 1370 cm⁻¹ to 1350 cm⁻¹ which is in accordance with a specific interaction and 317 318 confirmed that a formation of an outer-sphere hydrogen bonded complex is not the major adsorption 319 mode, so the structure (6) can be discarded. Finally, the intensity of the CH₂ (1440 cm⁻¹) bending mode is enhanced after the adsorption. This latter modification is attributed in the literature^{13,45} to a 320 321 geometrical constraint undergone by the CH₂ group that could be explained by the adsorption involving 322 the two carboxylic groups. This hypothesis would also be consistent with the neutralization observed in 323 the zetametry measurements. The Figure 6 (b) and (c) indicate that the drying slightly impacts the 324 geometry of the complex formed at the surface. The main difference between the two spectra is the 325 higher intensity of the CH₂ bending mode, which could be interpreted as a stronger geometric

326 constraint undergone by the CH₂ group and/or the presence of a symmetric COO stretching band under327 the latter.

328

The geometry of the complex can be refined using the difference between the asymmetric and symmetric stretching mode of COO as evocated by Dobson and McQuillan¹³. Indeed, this value is characteristic of the type of binding mode of the complex formed in solution or at the surface⁴⁰. Two adsorption modes of a carboxylic group can be distinguished, the bridging bidentate mode and the side on ester linkage with hydrogen bonding (Table 2), found in the adsorbed malonic complex 8-11 in Figure 4.

Table 2 : Adsorption mode of carboxylic acid group depending on the COO asymmetric and symmetric stretching mode
 difference

Bridging Bidentate	Side on Ester linkage
Δv(COO)	Δv(COO)
150-180 cm ⁻¹	> 208 cm ⁻¹

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338

339 The wavenumber difference between the COO asymmetric and symmetric stretching modes Δv (COO) varies from 150 to 180 cm⁻¹ for the bridging bidentate and is higher than 208 cm⁻¹ for the side on ester 340 341 linkage (208 cm⁻¹ being the value in the dissolved dianion). By applying this rule to the *in situ* spectrum 342 of adsorbed malonate (Figure 6 (b)), a difference of Δv (COO)=230 cm⁻¹ is found in agreement with 343 previous studies^{2,46}: both carboxylic moieties are mainly adsorbed through the same mode, the side on 344 ester linkage (Figure 4 (11)). The carboxylic moiety adsorbs by sharing a hydrogen atom with an oxygen 345 of the alumina surface, giving rise to a strong hydrogen bonding with similar features than carboxylate⁴⁷. This adsorption mode occurs directly at the wet interface and further drying stage 346 347 removing water molecules can impact the geometry of the complex and bonding mode, contrary to the 348 case of a bidentate bridging complex. Indeed, the spectra in Figure 6 (b) and (c) are slightly different. After the drying stage, a value for Δv (COO) of 166 cm⁻¹ could be measured, considering that the 349 350 symmetric COO stretching is shifted towards higher wavenumbers at 1430 cm⁻¹. This indicates that the 351 adsorption involved both a side-on ester linkage and a bidentate bridging mode after the drying of the 352 solid in the same adsorption mode (Figure 4 (10)) or present in the several modes (Figure 4 (8) and 353 (11)).

The adsorption mode has been determined during the equilibrium adsorption of the malonic acid as well as after a drying stage. Combining adsorption isotherm, zetametry measurements and ATR-FT-IR

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356 characterizations, adsorption modes (1)-(7) and (9) have been discarded while three modes (8), (10) and

357 (11) have been identified as possible structures of surface complex (Figure 4), with speciation being

influenced by the drying stage. However, this drying influence seems absent when the impregnation is

359 performed at a pH higher than pKa_2 as illustrated on the Figure 7.





363 Surprisingly, the pH seems to slightly impact the complex geometry after a drying stage which was not 364 the case at the wet interface (Figure 2). It can be observed that a shoulder is developed at higher 365 wavenumbers around 1600 cm⁻¹ for the asymmetric stretching mode of COO only at pH 4. This shoulder development is concomitant with the increasing intensity of the band situated at 1430 cm⁻¹ assigned to 366 the CH₂ bending mode. This observation is a strong indication of the contribution of both the CH₂ 367 368 bending mode as well as the COO symmetric stretching mode to the 1430 cm⁻¹ band. The shoulder is 369 absent for a pH above the second pKa (pKa₂=5.7) for supports impregnated by IWI and dried at 120°C for 6 hours. These observations can be linked to solution speciation. Indeed, at the impregnation 370 conditions (2.9 mol L^{-1} and pH 4), the monoacid form is the major species in solution, while the 371 372 malonate (dianionic form) is the major one for a pH higher than pKa₂. During the impregnation, the 373 buffer effect of the surface is expected to be strongly reduced by the high concentration of the malonic 374 acid. The evolution of the pH has been simulated using PhreeqC, and the results have shown that it would evolve from 4 to 4.6 in presence of malonic acid, whereas it would reach 6.8 without it. The 375 broadening of the band around 1600 cm⁻¹ could thus indicate an asymmetry of the two carboxylic 376 377 groups present in the molecule at pH 4 leading to two different binding modes, the ester linkage mode 378 with an hydrogen bond due to the carboxylate group and the bridging bidentate mode due to the 379 carboxylic group. These adsorption modes can either be present in the same adsorption mode 380 (structure (10), Figure 4) and/or in two different modes (structure (8) or (11), Figure 4).

381 As a result of the characterization techniques used, it has been seen that malonic acid adsorbs specifically at the alumina surface through the formation of a neutral complex involving the two 382 383 carboxylic functions which leads to a geometric constraint on the CH₂ group by formation of both 384 bidentate bridging and ester linkage mode. Consequently, only 3 remaining adsorption modes can 385 correspond to these observations for impregnation at pH 4 (structures (8), (10) and (11), Figure 4). The 386 malonic acid reacts with one or different alumina surface hydroxyls to specifically adsorb at the surface. 387 Consequently, in order to fully describe the surface chemistry after modification, the determination of 388 the surface hydroxyls involved in the modification is necessary. To achieve this description, an 389 experimental technique (FT-IR) is merged with a surface complexation model at the alumina surface.

390 At an atomic scale, experimental works have shown the presence of various surface sites, especially by the use of infrared spectroscopy. Morterra and Magnacca⁴⁸ showed the contribution of up to seven OH 391 392 groups. These surface hydroxyls are different by the charge developed which depends on the number of 393 bonds between the oxygen atom and aluminium atom(s) as well as on the aluminium coordination (tetra-coordinated, penta-coordinated and hexa-coordinated). Research works from Digne et al. 28,29 394 395 allowed a construction of a description model of the y-Al₂O₃ surface using DFT calculations which is 396 compared to an extensive list of published experimental data. The published model considers three 397 faces developed at the surface, (110), (100) and (111). The different types of hydroxyls can all be 398 considered as potential adsorption sites for malonic acid.

399 The spectra of dried samples have been recorded for malonic acid coverage from 0 up to 0.9 at/nm²

400 (Figure 8) after an activation at 120°C under vacuum (<10 $^{-5}$ mbar) in order to avoid the decomposition

401 of the organic at higher activation temperature. All spectra present large bands at 3770, 3752, 3730 and

402 3673 cm⁻¹ attributed Digne *et al.*^{28,29} respectively to the μ_1 -Al_{VI}-OH (100), μ_3 -Al_{VI}-OH (111), μ_1 -Al_V-OH

403 (110) and μ_2 -Al_V-OH (110).



405 Figure 8 : Transmission FT-IR spectrum of γ-Al₂O₃ samples after malonic acid sorption and activation at 120 °C under vacuum (10⁻⁵ mbar), OH stretch region

404

408 The decrease of the intensity of all bands observed on the Figure 8 seems to indicate that all surface hydroxyls corresponding to bands between 3650 and 3800 cm⁻¹ are involved in the adsorption of 409 410 malonic acid (see also the difference spectra in the supporting information, Figure S1). Only one band, at 3752 cm⁻¹ seems to grow a little but it could be explained by the decrease of the overlapping 411 412 neighbouring bands. However, at the monolayer coverage, infrared bands are still present, i.e. they are 413 not fully consumed confirming that the maximum coverage of the adsorbate is smaller than the surface 414 hydroxyl density⁴⁹. Due to the presence of residual water molecules at the surface, the resolution of the 415 bands is not very high and a detailed interpretation of the spectra is delicate. The crucial information 416 obtained from these spectra is the consumption of several surface hydroxyls present on two main 417 facets of alumina, (110) and (100). However, the description of the surface sites involved in the 418 adsorption of malonic acid cannot be directly derived from the FT-IR spectra alone, as the hydroxyl 419 sites' density and reactivity are very sensitive to the hydration state of the surface. The hydration state 420 corresponding to FT-IR conditions is different from the one encountered during the wet impregnation 421 process, hence the nature of the surface OH groups is not the same and the coordination sphere of the 422 surface Al atoms changes. When it comes to rationalize surface complexation phenomena according to 423 the so-called MUSIC complexation model^{37,50}, the protonation constants of surface hydroxo groups 424 depend on the local charge thus, on the coordination number of the host surface cations holding these 425 reactive groups. Consequently, the use of a surface complexation model involving a hydrated alumina 426 surface is necessary to identify the hydroxyls responsible for the adsorption at the solid/liquid interface.

427 The model of γ -alumina hydrated surface used in this surface complexation model is the one developed by some of us in reference ³² from the simulation of the acid-base titration curve of the surface. This 428 model is based on DFT information^{28,29} (density and charge of each site) and the MUSIC model^{51,52} to 429 430 determine the pKa of each hydroxyl site (Table S1 and S2 in the supporting information). The model 431 includes the two most developed facets on the alumina surfaces, the (100) and (110) orientations, in their respective proportion^{28,53} (20 and 80% respectively) and with their hydroxyl content and structure 432 433 at the solid/liquid interface. The main differences, between the model that is relevant at FT-IR 434 conditions and the one used here for the interpretation of zetametry experiments, are a higher OH 435 content and the full saturation of the coordination spheres of surface Al sites in the latter model, which 436 influences the surface protonation constants. Moreover, to describe the complete solid/solution 437 surface charge as a function pH, all this information has been implemented into surface speciation calculations made by means of the PHREEQC2 software⁵⁴ and applying a basic Stern double layer model. 438

439 Our model considers several hypotheses based on the literature and on our results obtained by surface 440 characterization experiments. Firstly, no protonation/deprotonation constant has been implemented 441 on the adsorbed surface complex due to the neutrality plateau observed by zetametry experiments in 442 the pH range between 5.5 and 8.0 (Figure 5) and the participation of the two carboxylic groups 443 according to ATR-FT-IR (Figure 6 and Table 2). Secondly, malonic acid adsorption is considered as 444 irreversible due to its specific adsorption, since only a small quantity of malonate adsorbed is released 445 after an application of a drying stage and a washing stage regardless of the pH of the washing solution 446 (Figure S3).

The use of this model does not imply any fitting procedure as the main objective is to reproduce the evolution of the zetametry curve with increasing malonate content. Thus, by comparing our data with scenarios implying a specific and successive consumption of surface sites, we firstly aim to simulate the neutralization plateau observed in zetametry and secondly model the curve progression of the experimental zetametry measurements observed in Figure 5.

- Several scenarios have been tested to retrieve the characteristic neutralization plateau observed at the monolayer coverage during the zetametry measurements (Figure S2). The curve in Figure 9 represents the closest simulation to the experiment. Some differences exist between simulated and measured zeta potential curves which mostly consists in a shift of surface charge at pH above 8, i.e. in the domain where the malonate adsorption becomes negligible. This difference already existed in the original model (where only the (de)protonation of the hydroxyl groups was simulated) and has no impact for the determination of the geometry of the malonate surface complex.
- To obtain the plateau (Figure 9), we had to distinguish between the reactivity of the two facets of γ -Al₂O₃ particles. Thus, all the hydroxyl sites on the (100) facet need to be involved whereas only the μ_1 -Al-OH (IV and VI) of the (110) facet are consumed by the adsorption (Table 3). The involvement of these two latter sites is not surprising as they are one the most basic (reactive) surface hydroxyls. The total density of surface sites involved is 3.2 OH/nm² corresponding to 3.5 OH/molecule adsorbed (with 0.9 molecule/nm² as monolayer coverage content) which is coherent with the structure mode ((8) and (10),

- 465 Figure 4) since the surface complexes formed consume between 3 (structure 10)) and 4 (structure (8))
- 466 surface hydroxyls.
- 467Table 3 : Characteristics of γ-Al2O3 surface -OH groups at different malonic acid coverage (from 0 to 100%) for the (100) and468(110) orientations taking into account the facets proportion.

	Surface sites density (at/nm ²)														
		(100)			(110)										
Surface Coverage	μ1-Alvi	μ₂-Alvı- Alıv	μ₃-Al _{vı}	μ1-Alıv	μ1-Alvi	μ₂-Al _{vi} - Al _{iv}	μ₂-Al _{vı} - Al _{vı}	μ₃-Al _{vı}							
0%	0.43	0.22	0.22	1.19	1.19	2.38	1.19	1.19							
20%	0.35	0.17	0.17	0.95	0.95	2.38	1.19	1.19							
40%	0.26	0.13	0.13	0.71	0.71	2.38	1.19	1.19							
60%	0.17	0.09	0.09	0.48	0.48	2.38	1.19	1.19							
80%	0.09	0.04	0.04	0.24	0.24	2.38	1.19	1.19							
100%	0.00	0.00	0.00	0.00	0.00	2.38	1.19	1.19							



470

471 Figure 9 : Evolution of the ζ potential as a function of pH for alumina modified by malonic acid compared to experimental
 472 data

473

474 The second information that the model can illustrate here is the reactivity of the sites involved in the 475 monolayer coverage formation. Indeed, it has been highlighted that only the consumption of specific 476 surface sites allows retrieving the evolution of the zetametry curves as a function of increasing surface 477 coverage observed experimentally (Figure 10). Concerning the adsorption sites needed to model the 478 plateau, the results indicate that none of these adsorption sites are more reactive than the others (the 479 average site consumption as a malonic acid coverage increases is the same for all sites), as only a 480 continuous decrease of all sites involved makes it possible to retrieve the curves' evolution. This result is 481 consistent with FT-IR data where the evolution of the different bands as function of malonate content 482 shows a continuous decrease. Thus, according to these results, the involved sites present similar reactivity. However, the consequences of malonic acid adsorption, and the resulting surface properties 483

484 after the adsorption process, are expected to be different for the two facets: in the (100) orientation all

485 OH groups are consumed whereas in the (110) facet only two μ 1 sites are involved and the remaining 486 μ 2 and μ 3 remain unconsumed.

487



489 Figure 10 : (A) Zeta potential as a function of pH for different contents of malonic acid from 0 to 0.9 molecule/nm² (lines are used as guidance for the reader) (B) Calculated ψ1 as a function of pH for different content of surface hydroxyls consumed (from 0 to 3.2 OH/nm²)

492

493 Consequently, the model presented here supports the determination of the complex adsorption modes 494 obtained by experimental characterization but also helps to get more specific information on the 495 adsorption process by identifying the surface hydroxyls involved in the adsorption and their reactivity. 496 To the best of our knowledge, this is the first time the adsorption of malonic acid (carboxylic acid) is so 497 deeply characterized by both its surface complex geometry and the sites responsible for its adsorption.

498

499 Conclusion

The complementarity between the use of multi-technique characterization and modelling has been 500 501 demonstrated here by the description at the molecular level of a modified γ -Al₂O₃ surface with malonic 502 acid. The surface complex geometry was determined via the coupling of adsorption isotherm, zetametry 503 measurements and ATR-FT-IR characterization. The complex involves two types of carboxylate bonding, 504 bridging bidentate and side-on ester linkage leading to a neutral complex at the surface. The infrared 505 characterization even underlined a slight drying effect on the geometry of the adsorbed complex 506 probably due the removal of water molecule. The results presented here show that the progressive 507 coverage of the surface by malonic acid complex neutralized the surface once the monolayer coverage 508 content of 0.9 molecule/nm² is achieved by the consumption of specific surface sites. The whole (100) 509 facet is reactive towards the adsorption while only μ_1 -Al_{VI}-OH and μ_1 -Al_{IV}-OH are involved on the (110) 510 facet. It also helps to support the complex geometry defined via experimental infrared data, i.e. a

511 consumption of 3.5 OH/molecule, in coherence with the two proposed structures for the adsorption 512 mode.

513 This work helps to obtain a high level of detail on the adsorption of a dicarboxylic acid on an oxide 514 surface by including the monolayer coverage content, the surface sites and facets involved in the 515 adsorption and the surface complex geometry. The molecular description of the modified alumina 516 surface will allow the preparation of catalyst with defined surface chemistry, a useful strategy to 517 understand the impact of the latter during the different preparation steps and on the catalytic 518 performance.

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Malonate speciation at γ-alumina surface using surface complex modelling based on a multi-technique characterization approach

667 Teddy Roy, Manuel Corral Valero, Thibaut Corre, Olivier Delpoux, Gerhard Pirngruber, Grégory Lefèvre



- Figure S1 : Transmission FT-IR difference spectra between γ-Al₂O₃ and alumina impregnated with malonic acid at different
 content (from 0.2 to 0.9 at/nm²) after activation at 120°C under vacuum (10⁻⁵ mbar), OH stretching region.

- 678 orientations¹

		Surface density (nm ⁻²)							
OH site	Al involved	(100)	(110)						
H ₂ O	Alvi	2.17	4.48						
μ_1	Alvi	2.17	1.49						
μ_1	Al _{IV}	0	1.49						
μ_2	AI_{VI} and AI_{IV}	1.09	2.98						
μ_2	Only Al _{vi}	0	1.49						
μ₃	Only Al _{VI}	1.09	1.49						

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Table S2: Calculation of Protonation Constants Using AIMD Simulations To Determine the Number of H Bonds around
 Oxygen Atoms in Hydroxyl Groups (a + d) and the number of H bonds around their respective protons (p)¹

OH site	Al involved	Protonation reaction	Log K	Nb of H bonds with the proton										
	Surface (100)													
μ_1	Alvı	$\mu_1 OH^{-0.5}$ + $H^+ \leftrightarrows \mu_1 OH_2^{+0.5}$	8.16	0.86										
μ_2	$AI_{VI} - AI_{IV}$	$\mu_2 O^{-0.75}$ + H ⁺ \leftrightarrows $\mu_2 O H^{+0.25}$	10.32	n.a.										
μ_3	Alvi	$\mu_3 O^{-0.5}$ + H ⁺ \leftrightarrows $\mu_3 O H^{+0.5}$	5.94	n.a.										
Surface (110)														
μ_1	Al _{IV}	$\mu_1 OH^{-0.25}$ + $H^+ \leftrightarrows \mu_1 OH_2^{+0.75}$	0.12	0.75										
μ_1	Al _{IV}	$\mu_1 O^{-1.25} + H^+ \leftrightarrows \mu_1 O H^{-0.25}$	12.97	n.a.										
μ_1	Alvi	$\mu_1 O H^{-0.5} + H^+ \leftrightarrows \mu_1 O H_2^{+0.5}$	9.16	0.95										
μ_2	Al _{VI} - Al _{IV}	$\mu_2 O^{-0.75} \textbf{+} \textbf{H}^{+} \leftrightarrows \mu_2 O \textbf{H}^{+0.25}$	10.45	n.a.										
μ_2	AI_{VI} - AI_{VI}	$\mu_2 OH^0 + H^+ \leftrightarrows \mu_2 OH_2^{+1}$	0.29	0.57										
μ2	AI_{VI} - AI_{VI}	$\mu_2 O^{-1} + H^+ \leftrightarrows \mu_2 O H^0$	13.86	n.a.										
μ₃	Alvı	$\mu_3 O^{\text{-0.5}} + H^{\text{+}} \leftrightarrows \mu_3 O H^{\text{+0.5}}$	4.75	n.a.										



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686Figure S2: PHREEQC simulations of the $ψ_1$ evolution as a function of pH for different scenarios after surface sites removal of
the γ-Al₂O₃ model (φ = removal of sites of this face)







Figure S311 : Malonic acid content (molecule/nm²) obtained after a washing stage at different pH

692 PHREEQC Script

```
694
     TITLE CD-MUSIC alumina Malonic acid
695
696
     PHASES
697
     Fix H+
698
           H+ = H+
699
           log k 0
700
     SURFACE MASTER SPECIES
701
     Alo b Alo b0-1.5
702
     Alo c Alo c0-0.75
703
     Alo e Alo eO-0.5
704
705
     Alp a Alp a0-1.25
706
     Alp b Alp b0-1.5
707
     Alp c Alp cO-0.75
708
     Alp_d Alp_dO-1
709
     Alp e Alp e0-0.5
710
711
     SURFACE SPECIES
712
           # face (100)
713
714
    Alo b0-1.5 = Alo b0-1.5
715
     log k 0
716
     -cd music 0 0 0
717
718
     Alo bO-1.5 + Na + = Alo bONa-0.5
719
     log k -0.096
720
     -cd music 0 0 1
721
722
     Alo b0-1.5 + H + = Alo b0H - 0.5
723
     -cd music 1 0 0
724
     log k 20.6
725
726
     Alo bOH-0.5 + Na + = Alo bOHNa+0.5
727
     log k -0.096
728
     -cd music 0 0 1
729
730
     Alo bOH-0.5 + H+ = Alo bOH2+0.5
731
     -cd music 1 0 0
732
     log k 8.16 #8.72
733
734
     Alo bOH2+0.5 + Cl = Alo bOH2Cl-0.5
735
     log k -0.176
736
     -cd music 0 0 -1
737
738
     Alo cO-0.75 = Alo cO-0.75
739
     log k O
740
     -cd music 0 0 0
741
742
     Alo cO-0.75 + Na + = Alo cONa + 0.25
743
     log k -0.096
744
     -cd music 0 0 1
```

```
745
746
     Alo cO-0.75 + H+ = Alo cOH+0.25
747
     -cd music 1 0 0
748
     log_k 10.32
749
750
     Alo cOH+0.25 + Cl- = Alo cOHCl-0.75
751
     log k -0.176
752
     -cd music 0 0 -1
753
754
     Alo COH+0.25 + H+ = Alo COH2+1.25
755
     -cd music 1 0 0
756
     log k -2.64 #-1.56
757
758
759
     Alo COH2+1.25 + Cl - = Alo COH2Cl+0.25
760
     log k -0.176
761
     -cd music 0 0 -1
762
763
     Alo e0-0.5 = Alo e0-0.5
764
     log k 0
765
     -cd music 0 0 0
766
767
     Alo eO-0.5 + Na + = Alo eONa + 0.5
768
     log k -0.096
769
     -cd music 0 0 1
770
771
     Alo eO-0.5 + H+ = Alo eOH+0.5
772
     -cd music 1 0 0
773
     log_k 5.94
774
775
     Alo eOH+0.5 + Cl - = Alo eOHCl - 0.5
776
     log k -0.176
777
     -cd music 0 0 -1
778
779
     Alo eOH+0.5 + H+ = Alo eOH2+1.5
780
     -cd music 1 0 0
781
     log_k -9.84 #-5.94
782
783
     Alo eOH2+1.5 + Cl - = Alo eOH2Cl+0.5
784
     log k -0.176
785
     -cd music 0 0 -1
786
787
           # face (110)
788
789
790
     Alp a0-1.25 = Alp a0-1.25
791
     log k 0
792
     -cd music 0 0 0
793
794
     Alp aO-1.25 + Na + = Alp aONa-0.25
795
     log k -0.096
796
     -cd music 0 0 1
797
798
     Alp_aO-1.25 + H+ = Alp_aOH-0.25
```

```
799
     -cd music 1 0 0
800
     log_k 12.97
801
802
     Alp aOH-0.25 + Na+ = Alp aOHNa+0.75
803
     log k -0.096
804
     -cd music 0 0 1
805
806
     Alp aOH-0.25 + H+ = Alp aOH2+0.75
807
     -cd_music 1 0 0
808
     log_k 0.12 #1.09
809
810
     Alp aOH2+0.75 + Cl - = Alp aOH2Cl - 0.25
811
     log k -0.176
812
     -cd music 0 0 -1
813
814
     Alp b0-1.5 = Alp b0-1.5
815
     log k O
816
     -cd_music 0 0 0
817
818
     Alp bO-1.5 + Na + = Alp bONa-0.5
819
     log k -0.096
820
     -cd music 0 0 1
821
822
     Alp_bO-1.5 + H+ = Alp_bOH-0.5
823
     -cd music 1 0 0
824
     log k 21.22
825
     Alp bOH-0.5 + Na+ = Alp bOHNa+0.5
826
827
     log k -0.096
828
     -cd_music 0 0 1
829
830
     Alp bOH-0.5 + H+ = Alp bOH2+0.5
831
     -cd music 1 0 0
832
     log k 9.16 #9.34
833
834
     Alp bOH2+0.5 + Cl - = Alp bOH2Cl-0.5
835
     log k -0.176
836
     -cd music 0 0 -1
837
838
     Alp cO-0.75 = Alp cO-0.75
     log k 0
839
840
     -cd music 0 0 0
841
842
     Alp cO-0.75 + Na + = Alp cONa+0.25
843
     log k -0.096
844
     -cd music 0 0 1
845
846
     Alp_cO-0.75 + H+ = Alp_cOH+0.25
847
     -cd music 1 0 0
848
     log k 10.45
849
850
     Alp_cOH+0.25 + Cl = Alp_cOHCl-0.75
851
     log k -0.176
852
     -cd music 0 0 -1
```

```
853
854
     Alp cOH+0.25 + H+ = Alp cOH2+1.25
855
     -cd music 1 0 0
856
     log k -1.90 #-1.43
857
858
     Alp cOH+0.25 + Cl = Alp cOHCl-0.75
859
     log k -0.176
860
     -cd music 0 0 -1
861
862
     Alp_dO-1 = Alp_dO-1
863
     log k O
864
     -cd music 0 0 0
865
866
     Alp dO-1 + Na+ = Alp dONa
867
     log k -0.096
868
     -cd music 0 0 1
869
870
     Alp_dO-1 + H+ = Alp_dOH
871
     -cd music 1 0 0
872
     log k 13.86
873
874
     Alp dOH + H+ = Alp dOH2+1
875
     -cd_music 1 0 0
876
     log_k 0.29 #1.98
877
878
     Alp dOH2+1 + Cl - = Alp dOH2Cl
879
     log k -0.176
880
     -cd music 0 0 -1
881
882
     Alp_eO-0.5 = Alp_eO-0.5
883
     log k O
884
     -cd music 0 0 0
885
886
     Alp eO-0.5 + Na + = Alp eONa + 0.5
887
     log k -0.096
888
     -cd music 0 0 1
889
890
     Alp eO-0.5 + H+ = Alp eOH+0.5
891
     -cd music 1 0 0
892
     log k 4.75
893
894
     Alp eOH+0.5 + Cl - = Alp eOHCl - 0.5
895
     log k -0.176
896
     -cd music 0 0 -1
897
898
     Alp eOH+0.5 + H+ = Alp eOH2+1.5
899
     -cd music 1 0 0
900
     log k -8.60 #-7.13
901
902
     Alp eOH2+1.5 + Cl - = Alp eOH2Cl+0.5
903
     log k -0.176
904
     -cd music 0 0 -1
905
906
```

```
907
     USER GRAPH
908
     chart title "charge de surface de l'alumine"
909
       -headings pH Alo bOH-0.5 Alo bOH2+0.5 Alo cO-0.75 Alo cOH+0.25 Alo eO-
910
     0.5 Alo eOH+0.5 charge Alo Alp aOH-0.25 Alp aOH2+0.75 Alp bOH-0.5
     Alp bOH2+0.5 Alp cO-0.75 Alp cOH+0.25 Alp dOH Alp eO-0.5 Alp eOH+0.5
911
912
     charge Alp psil Na ads Cl ads Alo pO-1.5 Alo pOH-0.5
913
      -connect simulations true
914
       -initial solutions false
915
       -axis titles pH sigma
916
       -axis scale x axis 2 12 2 1 # minimum 0, maximum 350, major tics at 50,
917
     minor tics at 25
918
           -axis scale y axis -8 -3 1
     #
919
      -start
920
     10 graph x -la("H+")
921
     30 graph sy mol("Alo bOH-0.5"), mol("Alo bOH2+0.5")
922
     40 graph sy mol("Alo cO-0.75"), mol("Alo cOH+0.25")
923
     60 graph sy mol("Alo eO-0.5"), mol("Alo eOH+0.5")
924
     70 graph y EDL("Sigma", "Alo")
925
     120 graph sy mol("Alp aOH-0.25"), mol("Alp aOH2+0.75")
926
     130 graph sy mol("Alp bOH-0.5"), mol("Alp bOH2+0.5")
927
     140 graph sy mol("Alp cO-0.75"), mol("Alp cOH+0.25")
928
     150 graph sy mol("Alp dOH")
     160 graph sy mol("Alp eO-0.5"), mol("Alp eOH+0.5")
929
930
     170 graph y EDL("Sigma", "Alp")
931
     200 graph y 0.32*EDL("psi1","Alp")+0.08*EDL("psi1","Alo")
     +0.6*EDL("psi1","Alpo")
932
     210 graph y 0.8*surf("Na","Alp")+0.2*surf("Na","Alo")
933
934
     220 graph y 0.8*surf("Cl", "Alp")+0.2*surf("Cl", "Alo")
935
     230 graph y EDL("psi1", "Alpo")
936
     240 graph_sy mol("Alo_pO-1.5"), mol("Alo_pOH-0.5")
937
       -end
938
939
     SOLUTION 1
940
         Na 100 charge; Cl 100
941
     SURFACE 1
942
         -sites units density # site concentration in sites/nm^2
943
          Alo b 0 40 1.0
                             # 2.17 40 2.0
944
          Alo c 0 # 1.09
945
          Alo e 0 # 1.09
946
947
          Alp a 0 160 1.0
                             #1.49
948
          Alp b 0 #1.49
949
          Alp c 2.99 # 2.99
950
           Alp d 0.25 # 1.49
951
           Alp e 1.49 # 1.49
952
953
     # Alo b moyen sur la particule : 2 site/nm2
954
955
         -capacitance 1.39 5
956
         -equilibrate 1
957
         -cd music
958
959
960
     EQUILIBRIUM PHASES; Fix H+ -2.8 HCl1 END
```

SOLUTION	2	;	pН	3	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-3	HCI	1	;	end
SOLUTION	3	;	рН	3.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-3.2	HCI	1	;	end
SOLUTION	4	;	рН	3.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-3.4	HCI	1	;	end
SOLUTION	5	;	рН	3.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-3.6	HCI	1	;	end
SOLUTION	6	;	pН	3.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-3.8	HCI	1	;	end
SOLUTION	7	;	pН	4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-4	HCI	1	;	end
SOLUTION	8	;	pН	4.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-4.2	HCI	1	;	end
SOLUTION	9	;	pН	4.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-4.4	HCI	1	;	end
SOLUTION	10	;	pН	4.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-4.6	HCI	1	;	end
SOLUTION	11	;	pН	4.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-4.8	HCI	1	;	end
SOLUTION	12	;	рН	5	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-5	HCI	1	;	end
SOLUTION	13	;	pН	5.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-5.2	HCI	1	;	end
SOLUTION	14	;	рН	5.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-5.4	HCI	1	;	end
SOLUTION	15	;	рН	5.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-5.6	HCI	1	;	end
SOLUTION	16	;	рН	5.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-5.8	HCI	1	;	end
SOLUTION	17	;	рН	6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-6	HCI	1	;	end
SOLUTION	18	;	рН	6.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM PHASES	;	Fix H+	-6.2	HCI	1	;	end
SOLUTION	19	;	pН	6.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-6.4	HCI	1	;	end
SOLUTION	20	;	pН	6.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-6.6	HCI	1	;	end
SOLUTION	21	;	pН	6.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-6.8	HCI	1	;	end
SOLUTION	22	;	рН	7	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-7	HCI	1	;	end
SOLUTION	23	;	рН	7.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-7.2	HCI	1	;	end
SOLUTION	24	;	рН	7.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-7.4	HCI	1	;	end
SOLUTION	25	;	рН	7.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-7.6	HCI	1	;	end
SOLUTION	26	;	pН	7.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-7.8	HCI	1	;	end
SOLUTION	27	;	pН	8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-8	HCI	1	;	end
SOLUTION	28	;	рН	8.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-8.2	HCI	1	;	end
SOLUTION	29	;	рН	8.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-8.4	HCI	1	;	end
SOLUTION	30	;	рН	8.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-8.6	HCI	1	;	end
SOLUTION	31	;	рН	8.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-8.8	HCI	1	;	end
SOLUTION	32	;	рН	9	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-9	HCI	1	;	end
SOLUTION	33	;	pH	9.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM PHASES	;	Fix H+	-9.2	HCI	1	;	end
SOLUTION	34	;	pH	9.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM PHASES	;	Fix H+	-9.4	HCI	1	;	end
SOLUTION	35	;	рН	9.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-9.6	HCI	1	;	end
SOLUTION	36	;	pН	9.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-9.8	HCI	1	;	end
SOLUTION	37	;	рН	10	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-10	HCI	1	;	end
SOLUTION	38	;	рН	10.2	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-10.2	HCI	1	;	end
SOLUTION	39	;	рН	10.4	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-10.4	HCI	1	;	end
SOLUTION	40	;	рН	10.6	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM_PHASES	;	Fix_H+	-10.6	HCI	1	;	end
SOLUTION	41	;	pH	10.8	;	Na	100	;	Cl	100	charge	;	USE SURFACE 1	;	EQUILIBRIUM PHASES	;	Fix H+	-10.8	HCI	1	;	end
			· · ·								U U										<u> </u>	

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